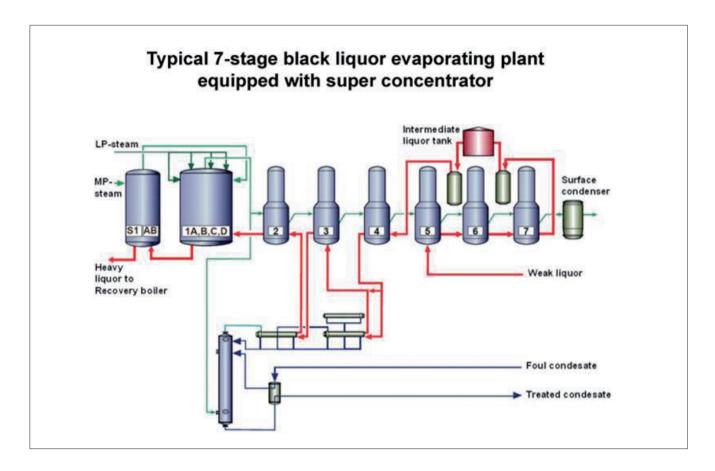


Valves in black liquor evaporation



Overview of the process

When processing wood chips into pulp in the cooking plant, organic materials dissolve in the cooking liquor. Black liquor contains both organic materials and also inorganic components of the cooking liquor.

The black liquor is separated from the pulp during the pulp washing. This weak black liquor (dry solids content of 14% - 18%) contains too much water for direct use as fuel in the recovery boiler.

The main purpose of the evaporation plant is to increase the dry solids content of the black liquor by evaporating water until reaching a concentration that allows burning in the recovery boiler. Since there is the potential danger of smelt explosions, the dry solids content of concentrated liquor should be a minimum of 58%.

Today a dry solids content of 72 ... 75 % is the minimum, and 80 ... 85% the target value for the dry solids content.

The process

An evaporation plant usually consists of several heat transfer units connected in series. A serie of evaporators is operated at different pressures to gain high steam economy.

Water removal is done by multiple effect evaporation in almost all pulp mills operating with the sulfate process. The number of effects is usually 5-7. The optimum number of effects depends on the steam balance of the mill.

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Requirements for valves

Black liquor is a thick media, which gets viscous when the dry solids content increases. Black liquor can cause scaling problems in the valve. Valves must be able to perform in both control and shut-off applications. Careful valve type selection is recommended for the last part of the evaporation plant and in pipes feeding the subsequent processes. When used in shut-off the valves must provide tight closure.

A flow diagram of six-stage evaporation plant is shown in the Figure 1. As the evaporation process moves from effect 6 toward effect 1, the solids content increases. Between effect 3 and effect 2 the solids content is above 50 %. Our valve recommendations can be seen in the Tables 1 and 2. The values mentioned in the Table 1 are typical average values of the evaporation processs. For control services the primary recommendation is the segment valve as well as the ball valve also. For lower solids content is the butterfly valve preferably used.

The operating conditions in the storage and evaporation of black liquor are moderately corrosive. Temperature rises approx. from 70 $^{\circ}$ C to 135 $^{\circ}$ C.

Rising solids content should also take into consideration when making the material selection Based on recent mill experiences Neles recommend to use duplex stainless steel material in the segment valve and ball valves if the solids content of black liquor is above 80 %. Otherwise grade 316 stainless steel in castings is sufficient.

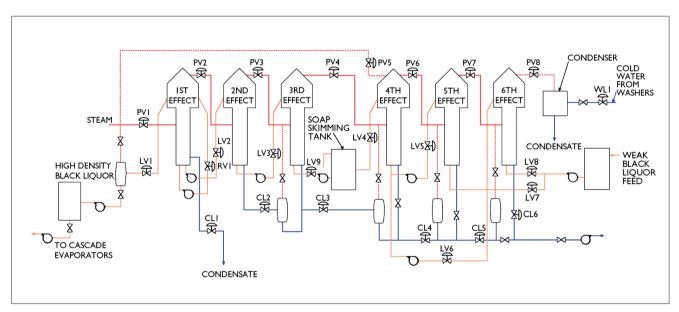


Fig. 1. Flow diagram of a multiple evaporator plant.

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Table 1. Process conditions of the evaporation plant and valve recommendations.

| Process variable | 1st effect | 2nd effect | 3rd effect | 4th effect | 5th effect | 6th effect |
|--------------------------|------------|------------|------------|------------|------------|------------|
| Temperature (°C) | 135 | 100 | 90 | | 75 | 65 |
| Specific gravity (kg/m³) | 1400 | 1200 | 1150 | 1120 | 1100 | 1050 |
| Solids content (%) | > 75 | | | | | 12-18 |

Values mentioned in the table are typical average values of the evaporation process.

| On-off valves | | | | | | |
|-----------------------------|---|--|--|--|--|--|
| Ball valve | * | | | | | |
| Triple eccentric disc valve | | | | | | |
| Control valves | | | | | | |
| V-port segment valve | * | | | | | |
| Ball valve | * | | | | | |
| Triple eccentric disc valve | | | | | | |

 $^{^{\}star}$ Duplex stainless steel is required if the solids content is above 80 %.

Table 2. Control valve selection of the evaporation plant.

| CONTROL VALVE SELECTION | | | | | | | |
|-------------------------|------------------------------|---|-----------------------------|---------------------------|--|--|--|
| Tag * | Application | Recommendation | Alternate | Typical size | | | |
| PV-1 to PV-8 | Steam pressure contol | V-port segment valve | Triple eccentric disc valve | DN200 (8") to DN300 (12") | | | |
| LV-1 and LV-2 | Liquor level control | V-port segment valve | Ball valve | DN100 (4") to DN200 (8") | | | |
| LV-3 to LV-8 | Liquor level control | Triple eccentric disc valve | V-port segment valve | DN150 (6") to DN200 (8") | | | |
| LV-9 | Soap skimming tank level | Triple eccentric disc valve V-port segment valve | DN150 (6") to DN200 (8") | | | | |
| RV-1 | Liquor recirculating control | V-port segment valve | Ball valve | DN100 (4") to DN200 (8") | | | |
| CL-1 to CL-6 | Condensate level control | Triple eccentric disc valve | V-port segment valve | DN100 (4") to DN200 (8") | | | |
| WL-1 | Water level control | V-port segment valve | Triple eccentric disc valve | DN80 (3") to DN150 (6") | | | |

 $^{^{\}ast}$ Tag numbers refer to the Figure 1.



Neldisc triple eccentric disc valve



V-port segment valve, series RA



M-series ball valve

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